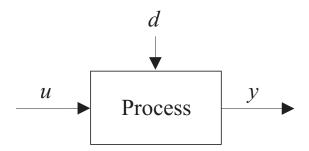
Conventional Control A Refresher

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Examples of "Processes"

- technical (man-made) system
- natural environment
- organization (company, stock exchange)
- human body
- ...

Process to Be Controlled



y : variable to be controlled (output)

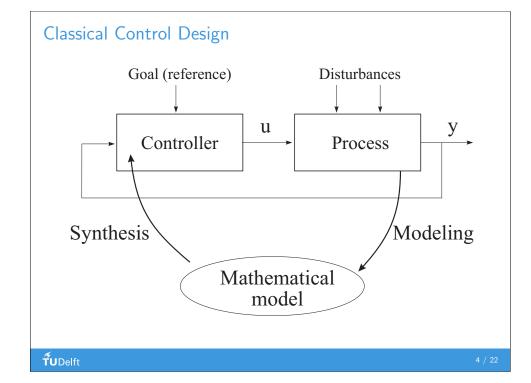
u : manipulated variable (control input)

d : disturbance (input that cannot be influenced)

dynamic system

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How to Obtain Models?

- physical (mechanistic) modeling
 - first principles → differential equations (linear or nonlinear)
 - 2 linearization around an operating point
- system identification
 - measure input-output data
 - 2 postulate model structure (linear-nonlinear)
 - 3 estimate model parameters from data (least squares)

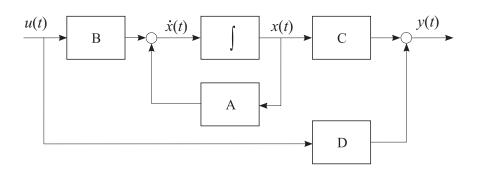
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Continuous-Time State-Space Model

$$\dot{x}(t) = Ax(t) + Bu(t)$$

 $y(t) = Cx(t) + Du(t)$



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Modeling of Dynamic Systems

x(t) ... state of the system

summarizes all history such that if we know x(t) we can predict its development in time, $\dot{x}(t)$, for any input u(t)

linear state-space model:

$$\dot{x}(t) = Ax(t) + Bu(t)$$

$$y(t) = Cx(t) + Du(t)$$

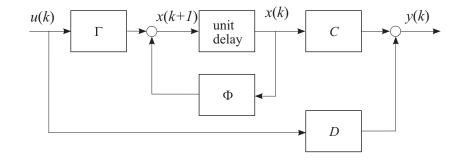
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Discrete-Time State-Space Model

$$x(k+1) = \Phi x(k) + \Gamma u(k)$$

$$y(k) = Cx(k) + Du(k)$$



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Input-Output Models

Continuous time:

$$y^{(n)}(t) = f\left(y^{(n-1)}(t), \dots, y^{(1)}(t), y(t), u^{(n-1)}(t), \dots, u^{(1)}(t), u(t)\right)$$

Discrete time:

$$y(k+1) = f(y(k), y(k-1), ..., y(k-n_y+1), ..., u(k), u(k-1), ..., u(k-n_u+1))$$

System Identification

Given data set

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$$\{(u(k), y(k)) \mid k = 1, 2, ..., N\}:$$

1 Postulate model structure, e.g.:

$$\hat{y}(k+1) = ay(k) + bu(k)$$

2 Form regression equations:

$$y(2) = ay(1) + bu(1)$$

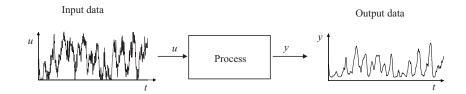
$$y(3) = ay(2) + bu(2)$$

:

$$y(N) = ay(N-1) + bu(N-1)$$

in a matrix form: $\mathbf{y} = \boldsymbol{\varphi}[a \ b]^T$

System Identification



$$u(1), u(2), \ldots, u(N)$$
 $y(1), y(2), \ldots, y(N)$

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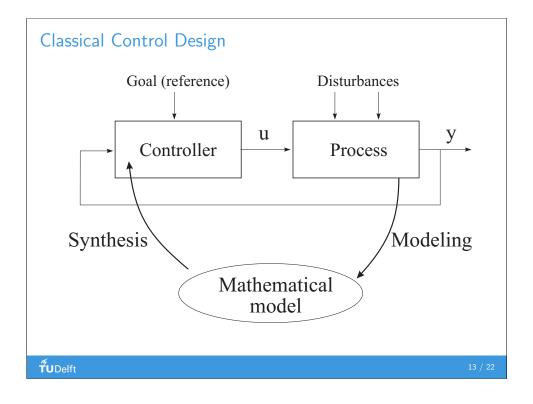
System Identification

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3. Solve the equations for [a b] (least-squares solution):

$$\mathbf{y} = \boldsymbol{\varphi} [\mathbf{a} \ \mathbf{b}]^T$$
$$\boldsymbol{\varphi}^T \mathbf{y} = \boldsymbol{\varphi}^T \boldsymbol{\varphi} [\mathbf{a} \ \mathbf{b}]^T$$
$$[\mathbf{a} \ \mathbf{b}]^T = [\boldsymbol{\varphi}^T \boldsymbol{\varphi}]^{-1} \boldsymbol{\varphi}^T \mathbf{y}$$

Numerically better methods are available (in Matlab [a b] = $\varphi \setminus y$).



Taxonomy of Controllers

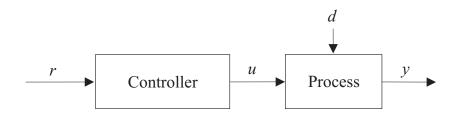
- Presence of feedback: feedforward, feedback, 2-DOF
- Type of feedback: output, state
- Presence of dynamics: static, dynamic
- Dependence on time: fixed, adaptive
- Use of models: model-free, model-based

Design Procedure

- Criterion (goal)
 - stabilize an unstable process
 - suppress influence of disturbances
 - improve performance (e.g., speed of response)
- Structure of the controller
- Parameters of the controller (tuning)

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Feedforward Control



Controller:

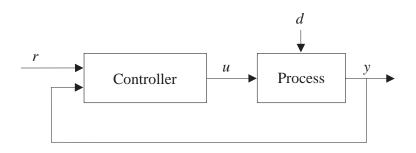
- (dynamic) inverse of process model
- cannot stabilize unstable processes
- ullet cannot suppress the effect of d
- sensitive to uncertainty in the model

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Feedback Control



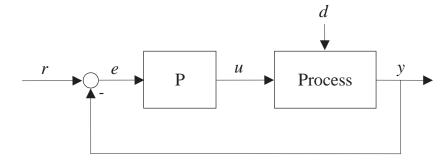
Controller:

- dynamic or static (\neq inverse of process)
- can stabilize unstable processes (destabilize stable ones!)
- ullet can suppress the effect of d

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Proportional Control

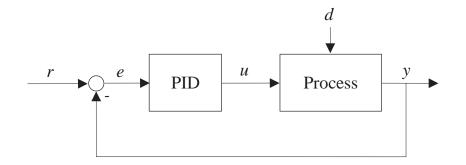


Controller:

• static gain P: u(t) = Pe(t)

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PID Control

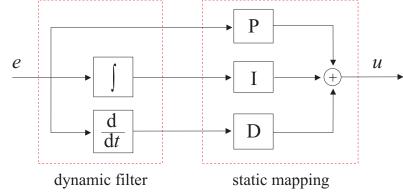


Controller:

- dynamic: $u(t) = Pe(t) + I \int_0^t e(\tau) d\tau + D \frac{de(t)}{dt}$
- P, I and D are the proportional, integral and derivative gains, respectively

PID Control: Internal View

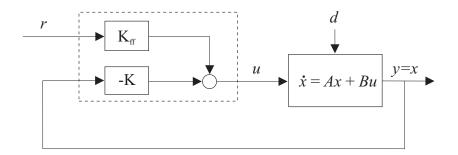
$$u(t) = Pe(t) + I \int_0^t e(au) d au + D rac{de(t)}{dt}$$



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State Feedback

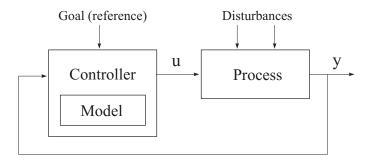


Controller:

- static: u(t) = Kx(t)
- K can be computed such that (A + BK) is stable
- $K_{\rm ff}$ takes care of the (unity) gain from r to y

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Model-Based Control



- state observer
- model-based predictive control
- adaptive control

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